

## Modelica based optimization - state of the art and future challenges

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![](_page_4_Picture_1.jpeg)

..."in practice there are relatively few optimization problems that can be solved efficiently. In many cases we can only hope to find a good-enough local optimum in finite search time, trading off between climbing hills in one place and looking for places that might have better hills to climb"

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Static optimization:

 Finding the <u>optimal point</u> (Euclidean space) to optimize a given objective function.

Dynamic optimization:

- Finding the <u>optimal control trajectories</u> over a time horizon to optimize a given objective function.
  - Trajectory optimization
  - Optimal control (=Optimalsteuerung)
  - Dynamic optimization/programming
  - MPC (Model Predictive Control). MPC is a control method based on repeated optimal control

#### General form of a dynamic optimization problem

minimize 
$$\phi\left(t_f, x(t_f)\right) + \int_{t_0}^{t_f} L(t, x(t), u(t))dt$$

 $s.t.F(t,\dot{x}(t),x(t),u(t)) = 0$  $x(0) = x_0$ Path constraints:  $g_i(x(t),u(t) \le 0$ Point constraints:  $g_e(x(t),u(t) = 0$ 

Solution strategies

#### <u>General form of a dynamic optimization problem</u>

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![](_page_17_Figure_1.jpeg)

**AEE INTEC** 

#### Polynomials approximate the variables of a DAE

The polynomials use the Lagrange basis polynomials, and they use the collocation points as the interpolation points.

$$\begin{aligned} x_i(\tau) &= \sum_{k=0}^{n_c} x_i \, \widetilde{l_k}(\tau), \quad y_i(\tau) = \sum_{k=1}^{n_c} y_i \, l_k(\tau), \\ \vdots \\ \dot{x}_i(\tau) &= \frac{dx_i}{d\widetilde{t_i}}(\tau) = \frac{d\tau}{d\widetilde{t_i}} \frac{dx_i}{d\tau}(\tau) = \frac{1}{h_i} \sum_{k=0}^{n_c} x_{i,k} \frac{d\widetilde{l_k}}{d\tau}(\tau) \end{aligned}$$

$$\widetilde{l_k}(\tau) = \prod_{\substack{l=0,\dots,n_c\\l\neq k}} \frac{\tau - \tau_l}{\tau_k - \tau_l}, \quad l_k(\tau) = \prod_{\substack{l=1,\dots,n_c\\l\neq k}} \frac{\tau - \tau_l}{\tau_k - \tau_l}$$

![](_page_18_Figure_1.jpeg)

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 $\widetilde{t_k}(\tau) = \prod_{\substack{l=0,\dots,n_c\\l\neq k}} \frac{\tau - \tau_l}{\tau_k - \tau_l}, \quad l_k(\tau) = \prod_{\substack{l=1,\dots,n_c\\l\neq k}} \frac{\tau - \tau_l}{\tau_k - \tau_l}$ 

The polynomials are defined on a finite number of collocation points. Hence, they **convert the infinite to a finite dimensional** optimization problem, which can be solved by a NLP solver

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## Why Modelica?

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### **General Trends**

- Previous studies have reported that the <u>time spending for</u> <u>model development</u> is significantly high (up to <u>80%</u>) [1-5]
- <u>70% of project costs</u> are consumed by <u>model creation</u> and calibration [6-8]
- There is an urgent need for <u>automated model creation</u> for optimization [10-12]

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#### **Declarative language**

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- Allow acausal modelling
- The order of the equations does not matter.

#### **Multi-domain modelling**

 Modelica is a multi-domain language, not geared towards any specific domain. Easily couple models containing for example, mechanical and electrical components.

#### **Object-oriented**

Models are classes and thus can easily be extended using ordinary object-oriented features.

#### Visual component programming

- Hierarchical system architecture capabilities.

#### Fully implicit DAE modelling approach

$$\mathbf{0}=F(t,x,\dot{x},y)$$

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## Modelica for optimization

#### Modelica is mainly intended for simulation

#### An extension to accommodate dynamic optimization problems is required

- Optimica: defines new syntax and semantics for specifying constraints and an objective
- Currently supported by JModelica.org, OpenModelica and IDOS

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#### Restrictions

- The most widely used numerical techniques for dynamic optimization are based on first-order necessary conditions for local optimality
  - The objective function and the DAE System must be twice continuously differentiable
  - Hybrid constructs are excluded!!!

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## Applications in the energy sector

- Optimal use of an electrochemical storage tank in combination with a MV photovoltaic
- Optimal start of a steam boiler
- Model predictive control of buildings
- Model predictive control of district heating systems
- Optimal start of a combined-cycle power plant

## Dynamic Optimization of a district heating system

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![](_page_29_Figure_2.jpeg)

min. 
$$\int_{t_0}^{t_f} (\alpha T_{\text{prod}} + \beta dp_{\text{prod}} + \gamma \dot{Q}_{\text{prod}}^2 + \delta dp_{\text{prod}}^2) dt,$$

s.t. model dynamics,

$$\begin{split} m_{Prod}(t) &\leq m_{Prod}^U \quad \forall t \in [t_0, t_f], \\ T_{Customer}^L &\leq T_{Customer}(t) \quad \forall t \in [t_0, t_f], \\ dp_{Customer}^L &\leq dp_{Customer}(t) \quad \forall t \in [t_0, t_f], \end{split}$$

![](_page_29_Figure_6.jpeg)

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- Complex dynamical effects
  - Producer increases supply temperature in advance
  - Temperature front propagates slowly
  - Customers close to producer benefit quickly from increased temperature
  - Customers at the periphery benefit from higher flowrates
- Optimization can handle
  - Flow-dependent delays
  - Slow temperature dynamics
  - Fast pressure/flow dynamics
  - Distributed network

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More Solver for dynamic optmization

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- <u>Mixed-integer-optimal control problems</u>

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- More domain specific libraries

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- <u>Mixed-integer-optimal control problems</u>
- More domain specific libraries
- Scalability studies

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Thank you for your Attention